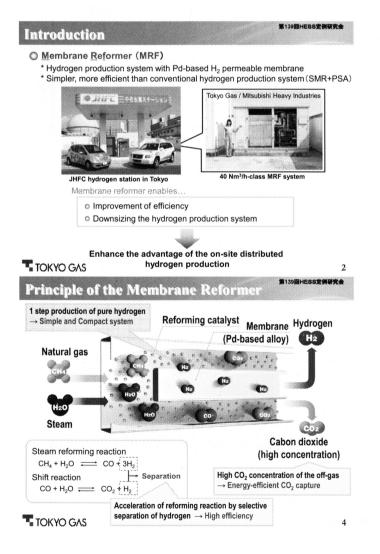
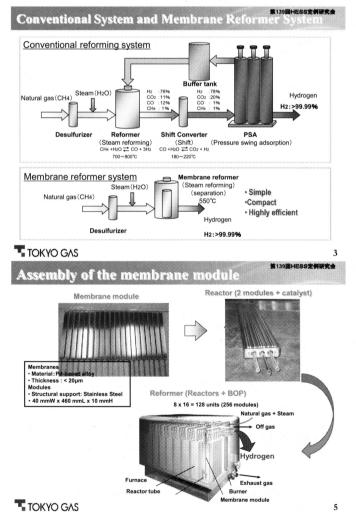
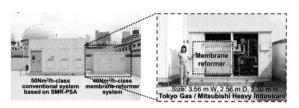
第 139 回定例研究会(2012WHEC 報告会) 資料 5







## 40 Nm³/h-class MRF (<u>M</u>embrane <u>R</u>eform



Developed the 40 Nm<sup>3</sup>/h class MRF system in 2003 and improved the performance in 2007.

○ Achievements

Efficiency: 81.4% (HHV) Capacity: 40.5 Nm3/h

Purity: 99.999% (5N)

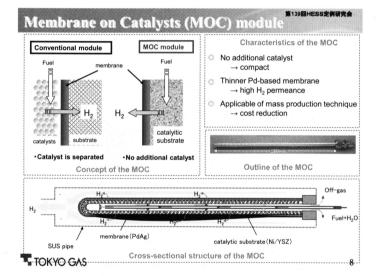
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- The efficiency of the MRF was improved by ... Increase the membrane area
- Improve heat recovery ·Use more efficient auxiliaries
- The efficiency of the 2<sup>nd</sup> MRF is over 80% and higher than the conventional hydrogen production system with PSA.

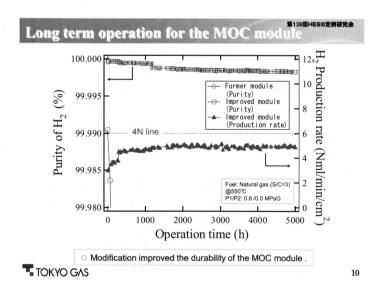
**Durability test** Load change test 100 100 90 90 Hydrogen production rate (Nm<sup>3</sup>/h) 80 80 70 Efficiency (%HHV) 60 60 & Conversion 50 50 Hydrogen production rate 40 40 30 30 20 20 10 10 P1/P2:0.8/-0.06 MPaG 0 0 1000 2000 4000 Time [h] Conversion, efficiency, and production rate are stable in the operation. For the mounted improved modules, no significant leakage has been detected.

Long term operation test for the 40 Nm<sup>3</sup>/h M

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## 第139個HESS定例研究会 Some causes of the leak on the MOC Some impurity particles Imperfection of the plating Mismatch of the materials at coming from the vessel react with Pd-membrane and make micro pores. process makes voids in the membrane. Coating a blocking material on the inner surface of the stainless vessel. Applying a glass-seal technique to the connection part between the module and Achieving perfect plating technique . the stainless pipe. TOKYO GAS



第139回HESS定例研究会 •The 40 Nm<sup>3</sup>/h class membrane reformer systems have been jointly developed with Mitsubishi Heavy Industries, Ltd. ·This work was supported by the New Energy and **Industrial Technology Development Organization** (NEDO). The authors acknowledge their supports. TOKYO GAS 11